

# The Behavior of Nitrogen Oxides in the $\text{N}_2\text{H}_4$ -NO- $\text{O}_2$ Reaction

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## INTRODUCTION

It has been discovered that  $\text{NH}_3$  selectively reduces NO in the presence of a large excess of  $\text{O}_2$  over the temperature range of 800 to 1,050°C (Lyon, 1976; Lyon and Benn, 1979). It has also been found that  $\text{H}_2\text{O}_2$  promotes the  $\text{NH}_3$ -NO reaction and initiates it at about 500°C (Azuhata et al., 1981, 1982). It is generally accepted that the selective reduction of NO with  $\text{NH}_3$  is attributed to the high reactivity of NO with  $\text{NH}_2$  and  $\text{NH}$  radicals, produced during the decomposition of  $\text{NH}_3$ , and the production of these radicals may be the key technology to reduce NO. Based on this philosophy, much effort has been devoted to finding more effective reducing agents than  $\text{NH}_3$  and/or additives that would promote the  $\text{NH}_3$ -NO reaction for the purpose of developing an NOx removal process from a combustion exhaust gas.

The main objective of this work was to determine if an ammonia derivative,  $\text{N}_2\text{H}_4$ , could reduce NO in the presence of a large excess of oxygen. While a significant number of experiments already has been performed on the decomposition of  $\text{N}_2\text{H}_4$  (Diesen, 1963; Michel et al., 1965; Meyer et al., 1969; Gehring et al., 1979), little information is available to access the applicability of  $\text{N}_2\text{H}_4$  to an NO reduction process.

## EXPERIMENTAL PROCEDURE

The experimental equipment and procedure were basically the same as those previously employed to study the reaction of  $\text{NH}_3$ -NO- $\text{H}_2\text{O}_2$  (Azuhata et al., 1982). The main change to the procedure in the present work was that, instead of  $\text{H}_2\text{O}_2$ , a water solution of  $\text{N}_2\text{H}_4$  was sprayed to fine droplets by a carrier stream of  $\text{N}_2$ . The sprayed liquid  $\text{N}_2\text{H}_4$  was vaporized at 120°C and then injected into an electrically heated quartz tube reactor 1.3 m long and 15, 20, and 40 mm I.D.

The flow rate of each reactant was measured with calibrated rotameters and the total flow rate was set at 100 mL/s (at 0°C and at atmospheric pressure). The content of  $\text{N}_2\text{H}_4$  in a gas mixture was controlled by varying the concentration of  $\text{N}_2\text{H}_4$  solution, and checked by the iodometric titration of hydrazinium sulfate, which was obtained by bubbling the sample gas through a dilute sulfuric acid. A Yanagimoto ECL 308 chemiluminescence NO/NOx analyzer was used to monitor NO and NO<sub>2</sub>. The composition of reactant mixture was 0–1,000 ppm  $\text{N}_2\text{H}_4$ , 0–200 ppm NO, 0–15%  $\text{O}_2$ , and  $\text{N}_2$  as carrier.

## EXPERIMENTAL RESULTS AND DISCUSSION

The influence of the reaction temperature on the  $\text{N}_2\text{H}_4$ -NO reaction was studied with and without  $\text{O}_2$ . Figure 1 shows the relation between reaction temperature and the concentration change of NO, NO<sub>2</sub>, and NOx (NO + NO<sub>2</sub>). The decrease in NO was observed above 500°C, in the absence of  $\text{O}_2$ . This result was easily predictable based on the kinetic data of the thermal decomposition of  $\text{N}_2\text{H}_4$  (Eberstein and Glassman, 1965), and NO was thought to be reduced to  $\text{N}_2$  and  $\text{H}_2\text{O}$  by  $\text{N}_2\text{H}_4$ .

In contrast, the presence of  $\text{O}_2$  prohibited the reduction of NOx.

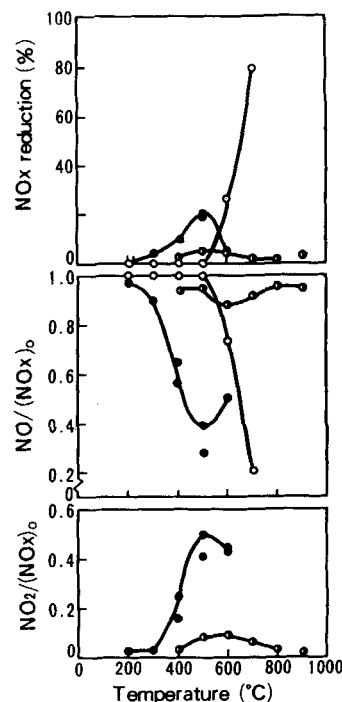


Figure 1. Variations of NOx reduction, NO, and NO<sub>2</sub> with reaction temperature in the  $\text{N}_2\text{H}_4$ -NO- $\text{O}_2$  reaction. Gas mixtures: 200 ppm  $\text{N}_2\text{H}_4$ , 200 ppm NOx (mostly NO but 0–5 ppm NO<sub>2</sub> as impurity), 0 ~ 15%  $\text{O}_2$ , balance  $\text{N}_2$ . ○:  $\text{O}_2$  absent; ◊: 3%  $\text{O}_2$ ; ●: 15%  $\text{O}_2$ .

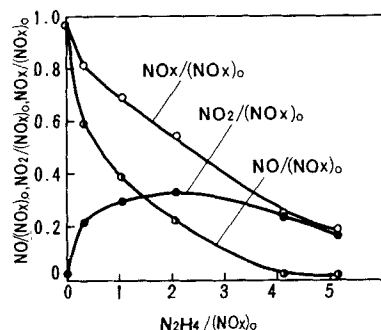


Figure 2. Relation between variations of NO, NO<sub>2</sub>, and NO<sub>x</sub> and initial molar ratio of N<sub>2</sub>H<sub>4</sub> with NO<sub>x</sub>. Gas mixtures: 0 ~ 1,020 ppm N<sub>2</sub>H<sub>4</sub>, 200 ppm NO<sub>x</sub> (195 ppm NO and 5 ppm NO<sub>2</sub>), 15% O<sub>2</sub>, balance N<sub>2</sub>. Temp., 500°C; reaction time, 0.4 s.

When 3% O<sub>2</sub> was added to the mixture of N<sub>2</sub>H<sub>4</sub> and NO, only a slight change in NO and NO<sub>2</sub> was observed. By increasing the O<sub>2</sub> concentration, the characteristic of the N<sub>2</sub>H<sub>4</sub>-NO-O<sub>2</sub> reaction became clearer. The marked result was the appearance of a large amount of NO<sub>2</sub>. Despite the large decrease in NO, NO<sub>x</sub> reduction was very low because of the formation of NO<sub>2</sub>. The NO<sub>2</sub> formation showed a large dependence on the O<sub>2</sub> concentration. About five times as much NO<sub>2</sub> was observed in the experiment with the 15% O<sub>2</sub> present as in that with 3% O<sub>2</sub>.

If NH<sub>2</sub> or NH radicals were to be produced in the N<sub>2</sub>H<sub>4</sub>-NO-O<sub>2</sub> reaction, a part of NO would have to be converted to N<sub>2</sub>. NH<sub>2</sub> was already proved to be highly reactive with NO, and the reduction of NO with NH<sub>3</sub> was well explained by assuming that NH<sub>2</sub> produced from NH<sub>3</sub> would react with NO in the presence of a large

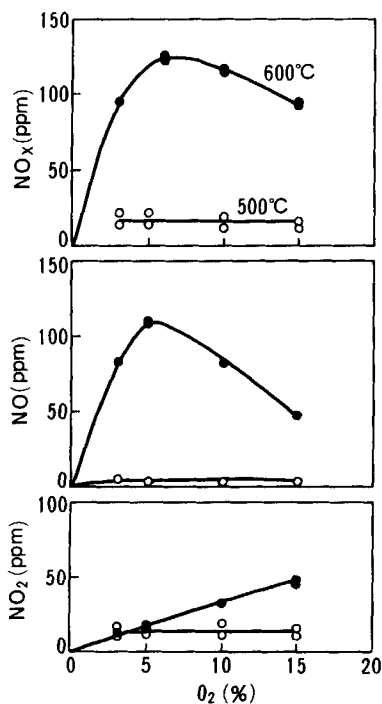


Figure 3. Formation of NO and NO<sub>2</sub> in the N<sub>2</sub>H<sub>4</sub>-O<sub>2</sub> reaction. Gas mixtures: 1,000 ppm N<sub>2</sub>H<sub>4</sub>, 3-5% O<sub>2</sub> balance N<sub>2</sub>. Temp., 500 and 600°C; reaction time, 0.4 s.

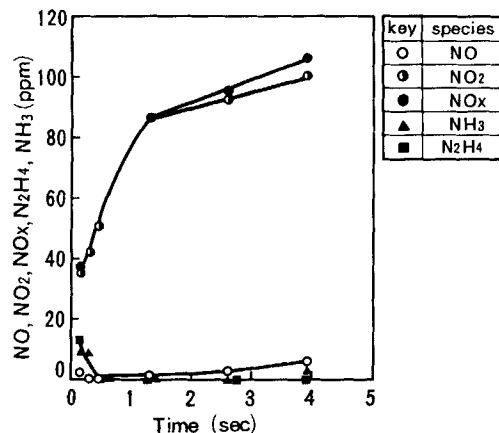


Figure 4. Variations of reactants with time. Gas mixture: 500 ppm N<sub>2</sub>H<sub>4</sub>, 100 ppm NO<sub>x</sub> (95 ppm NO and 5 ppm NO<sub>2</sub>), 15% O<sub>2</sub>, balance N<sub>2</sub>. Temp., 500°C.

excess of O<sub>2</sub> (Lyon and Benn, 1978; Azuhata et al., 1981). Therefore, the oxidation of N<sub>2</sub>H<sub>4</sub> with O<sub>2</sub> is thought to produce only a little amount of NH<sub>2</sub> or some intermediates that would react more rapidly with NH<sub>2</sub> than NO.

Figure 2 shows the influence of initial molar ratio of N<sub>2</sub>H<sub>4</sub> to NO<sub>x</sub> on the concentration change of nitrogen oxides. Experiments were conducted at 500°C with 15% O<sub>2</sub> present. The increase in N<sub>2</sub>H<sub>4</sub> caused the decrease in NO<sub>x</sub> and NO, and the NO<sub>2</sub> produced exhibited a weak dependence on N<sub>2</sub>H<sub>4</sub>.

In previous papers, little has been mentioned about the formation of NO<sub>2</sub> or about the reaction mechanism that would predict NO<sub>2</sub> formation. There are three plausible reaction pathways that will predict the NO<sub>2</sub> formation. The first possibility is the NO-O<sub>2</sub> reaction. But this reaction can be ruled out, because it was experimentally verified that the direct oxidation of NO with O<sub>2</sub> did not take place under the experimental conditions of this study. The second possibility is the oxidation of N<sub>2</sub>H<sub>4</sub> with O<sub>2</sub>, and the third is the oxidation of NO with some intermediates produced from the oxidation of N<sub>2</sub>H<sub>4</sub> with O<sub>2</sub>.

In order to confirm the relative importance of these two possible pathways, NO and NO<sub>2</sub> produced in the N<sub>2</sub>H<sub>4</sub>-O<sub>2</sub> reaction were measured. Figure 3 shows the formation of NO and NO<sub>2</sub> obtained when mixtures of 1,000 ppm N<sub>2</sub>H<sub>4</sub>, 0-15% O<sub>2</sub>, and N<sub>2</sub> as carrier were heated to 500 to 600°C. Both NO and NO<sub>2</sub> were detected due to the oxidation of N<sub>2</sub>H<sub>4</sub> with O<sub>2</sub>. A peak NO was observed around 5% O<sub>2</sub>, and NO<sub>2</sub> increased proportionally with O<sub>2</sub>, although the sum of NO and NO<sub>2</sub> showed only a slight dependence on O<sub>2</sub>. The experimental results in Figure 3 indicated that N<sub>2</sub>H<sub>4</sub> was converted to NO<sub>2</sub>, but the amount of NO<sub>2</sub> produced was 5% of N<sub>2</sub>H<sub>4</sub> at most at 600°C and below 2% at 500°C. These values were far less than those obtained in the reaction of N<sub>2</sub>H<sub>4</sub>-NO-O<sub>2</sub> shown in Figures 1 and 2. These experimental results would support the assumption that N<sub>2</sub>H<sub>4</sub> cannot be the main source of NO<sub>2</sub>, and NO<sub>2</sub> must be chiefly produced from NO.

Figure 4 shows the variations of N<sub>2</sub>H<sub>4</sub>, NO, NO<sub>2</sub>, and NH<sub>3</sub> with the reaction time. NO disappeared very rapidly, as did N<sub>2</sub>H<sub>4</sub>. A trace of NH<sub>3</sub>, which was the product of N<sub>2</sub>H<sub>4</sub> decomposition, was observed within 0.2 s. In contrast to these reactants, the formation of NO<sub>2</sub> occurred very slowly and continued for more than 1 s in the region where no N<sub>2</sub>H<sub>4</sub>, NH<sub>3</sub>, and NO could be detected.

These results suggest the assumption that the NO<sub>2</sub> formation in the N<sub>2</sub>H<sub>4</sub>-NO-O<sub>2</sub> reaction takes place in two distinct steps. The first rapid reaction of N<sub>2</sub>H<sub>4</sub> with NO proceeds in the presence of O<sub>2</sub> and yields a relatively stable species, which forms NO<sub>2</sub>. This reaction is followed by a slower reaction, which produces NO<sub>2</sub>.

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